Fuel Cell Modeling In AMESim

IMAGINE Specific Thermodynamic Applications 04/2006 Cédric ROMAN – roman@amesim.com



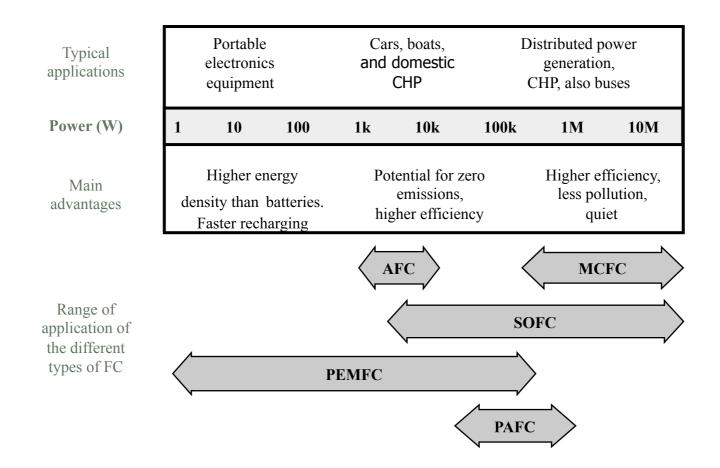


- Fuel Cells are complex multi-domain dynamic systems
 - Electrical, electrochemical, fluidic, thermal phenomena are coupled
 - Controlling such systems is a challenge to ensure efficiency and reliability
- Modelling fuel cells systems implies
 - Interoperability
 - Multi-disciplinary and dynamic simulation environment



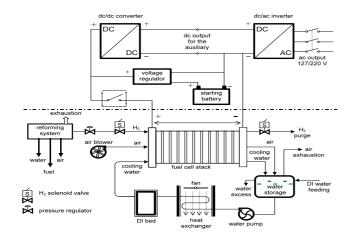


Power Based Fuel Cell Applications



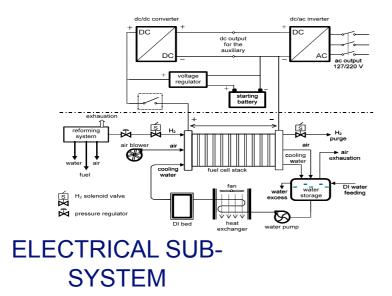






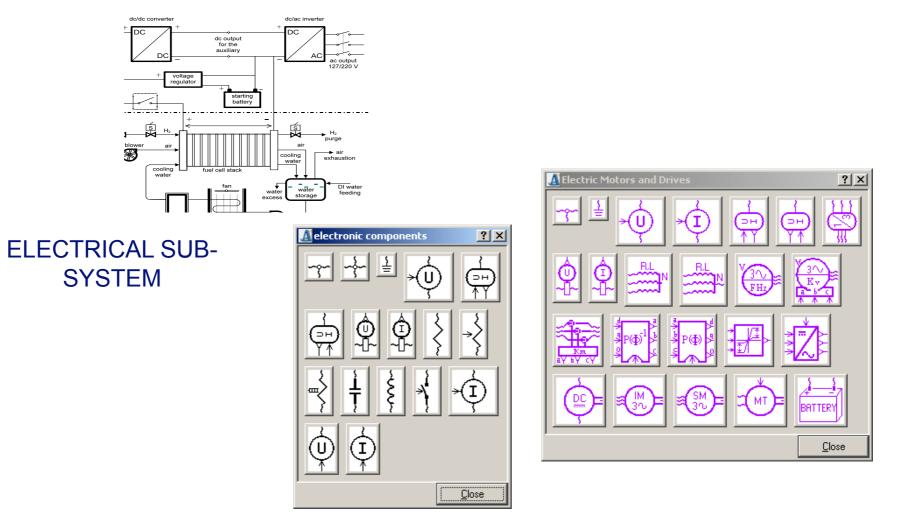






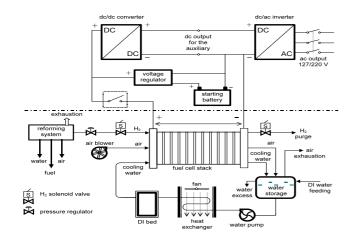








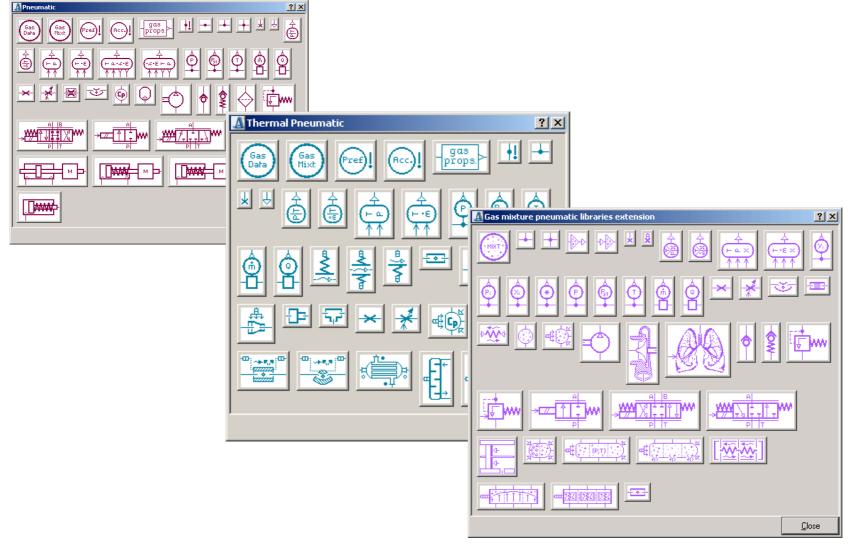




PNEUMATIC SYSTEM

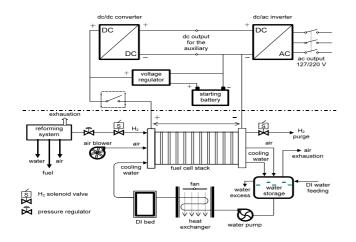










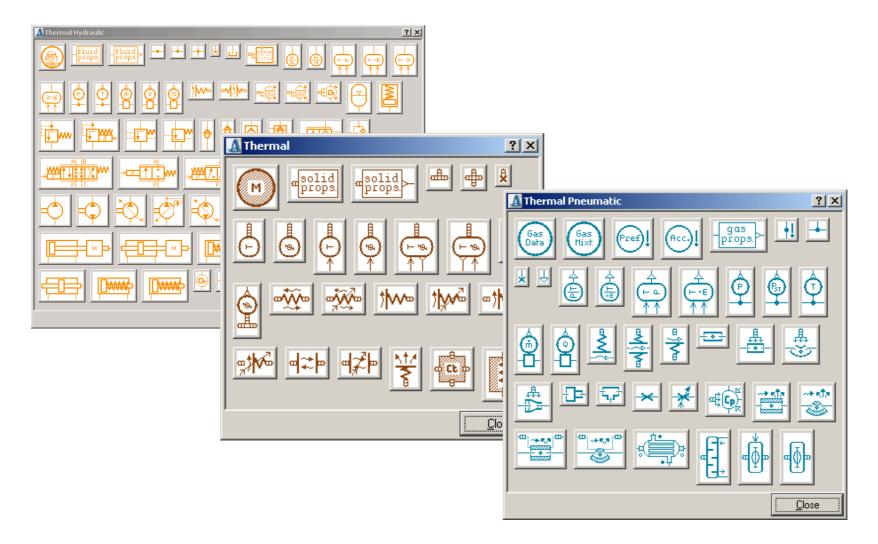


COOLING SYSTEM



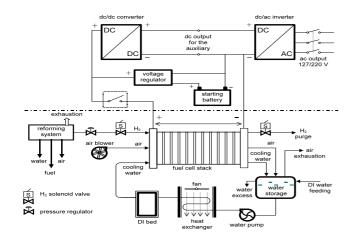












STACK SYSTEM





Introduction

 State of the art of PEMFC stack numerical models



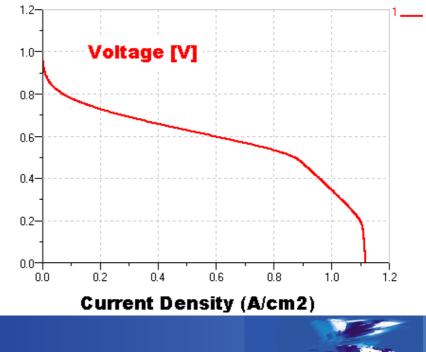
- Dynamic model of analogic electrical equivalent system
 - Pneumatics and chemicals are modelled with equivalent electric elements
- Quasi-steady state model based on CFD code
 - Limited by boundary conditions
 - CPU cost: days on parallelized clusters
- Bond-Graph model
 - Multi-domain (electrical/chemical/pneumatic)





Stack System

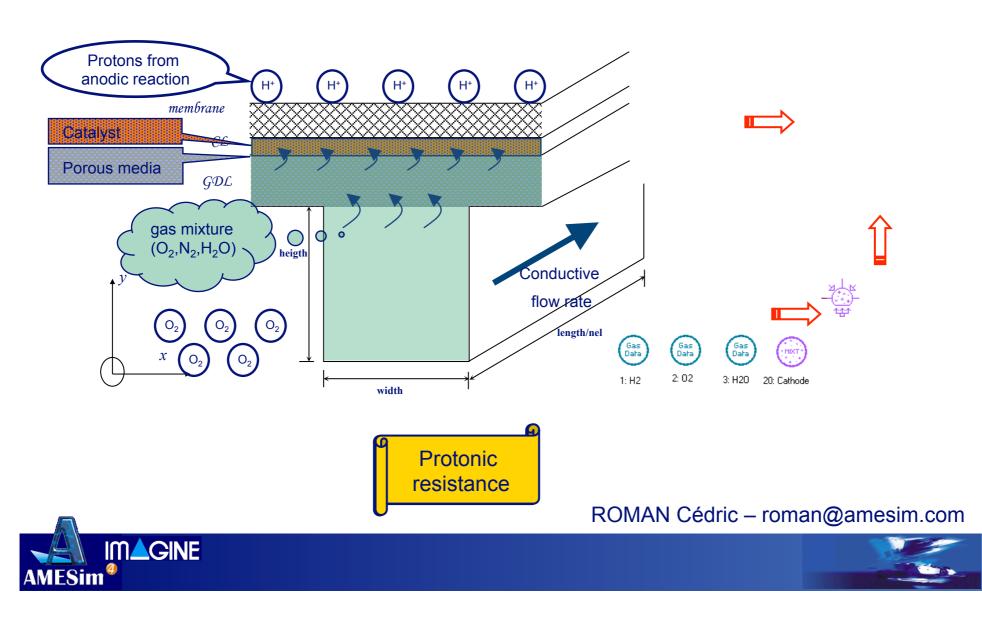
- AMESim Model for stack modelling
 - Inspired from Bond Graph
 - Physical model of electrical, electrochemical, pneumatic and thermal phenomena
 - Stack design and optimization
 - Dynamic modelling of pneumatics, chemical reactions, etc...





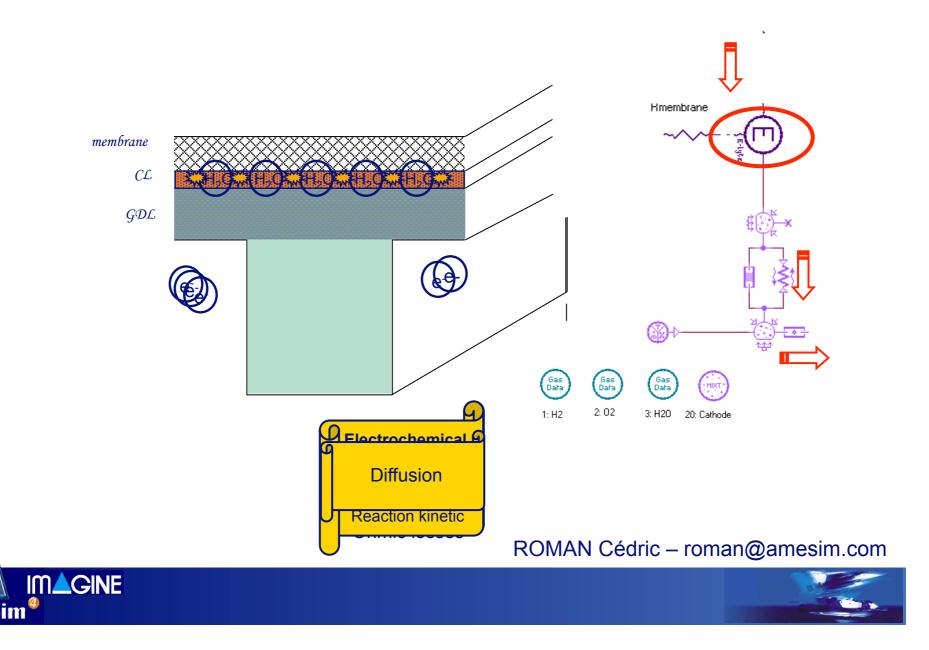
PEM cell Model structure (Explanations)

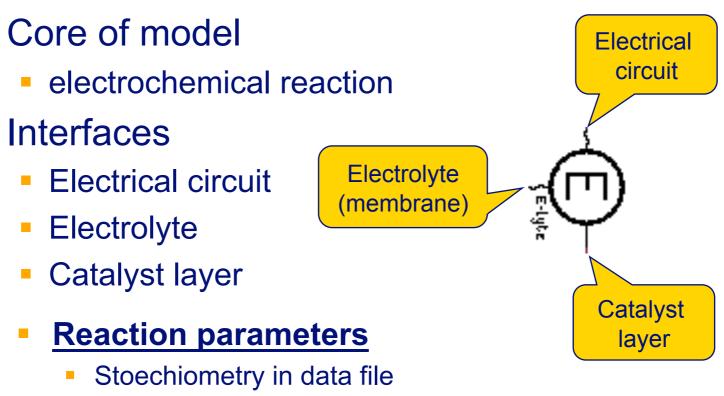
Cathode side



14

PEM cell Model structure (Explanations)





- Reference heat of formation, standard entropy
- Kinetic parameters in data file
 - Partial orders, kinetic constant
- Assymetry parameter
- ROMAN Cédric roman@amesim.com





PEMFC cathode

- Electrochemical reaction $O_2 + 4H^+ + 4e^- \Leftrightarrow 2H_2O$
- Gas mixture equilibrium potential
 - Nernst equation
- Overpotential
 - Activation Voltage
 - Equilibrium potential
 - = Disequilibrium
- Reaction kinetic
 - Butler-Volmer equation

 $\eta = U - E_{rev}$

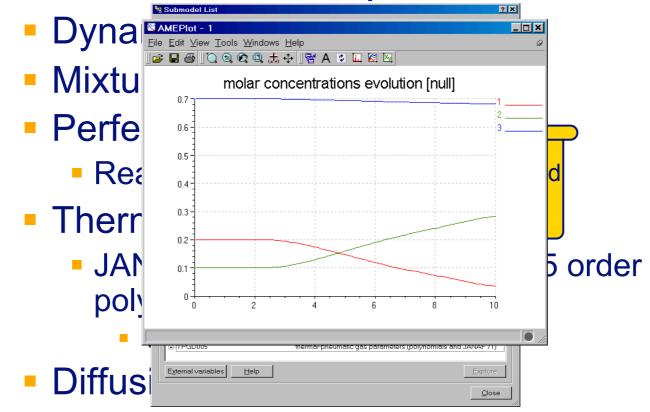
$$I = I_O \left[-\exp\left(-\alpha_C n \frac{F\eta}{RT}\right) + \exp\left(\alpha_A n \frac{F\eta}{RT}\right) \right]$$

 $E_{rev} = E^{o} - \frac{RT}{4 \cdot F} ln \left(\frac{a_{H_2O}^2}{a_{O_2} \cdot a_{H^+}^4 \cdot a_{e^-}^4} \right)$





Gas mixture description

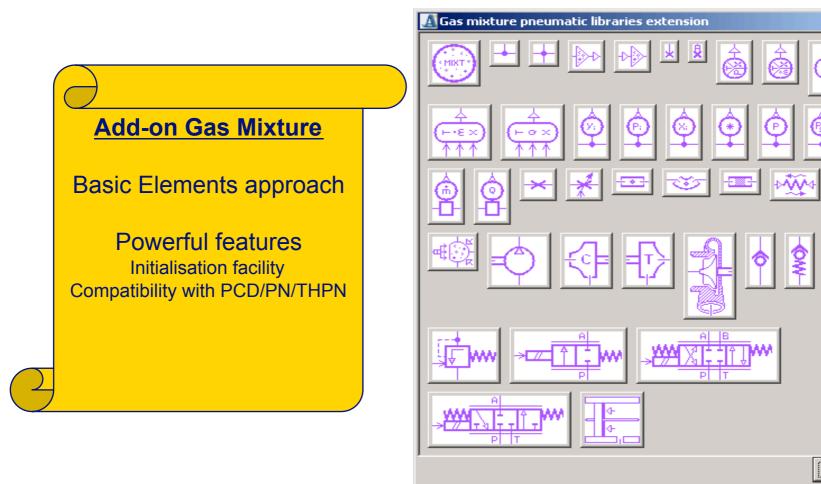


Binary coefficients / Wilke formula

• Water condensation/vaporisation (to come...)







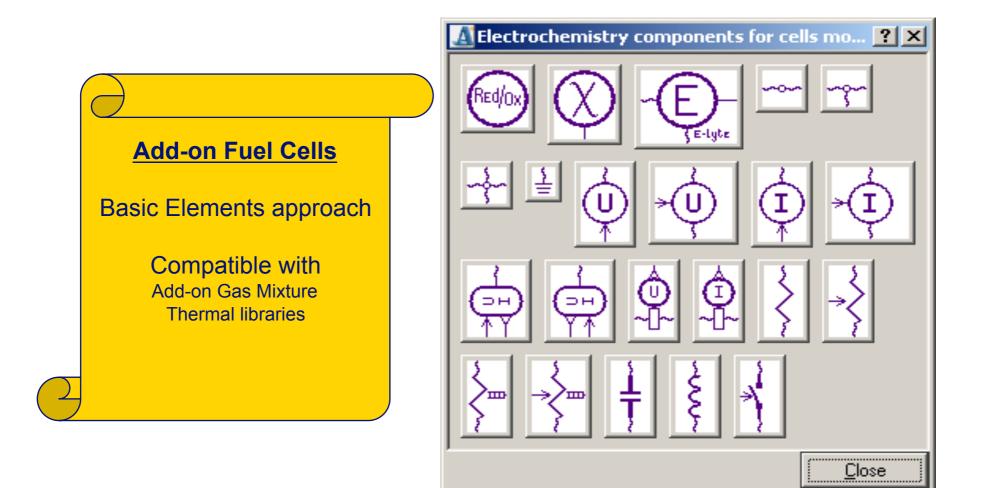
ROMAN Cédric – roman@amesim.com





<u>C</u>lose

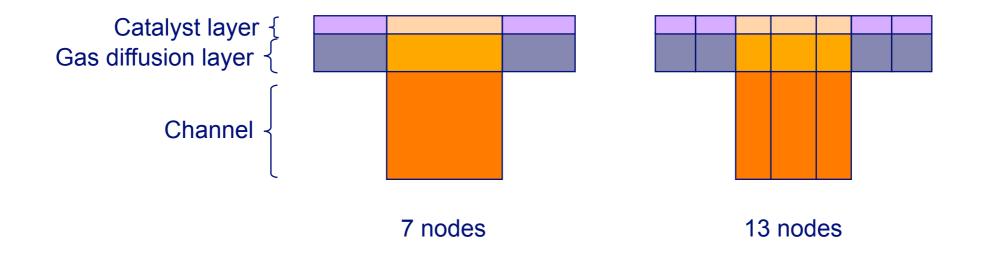
? ×





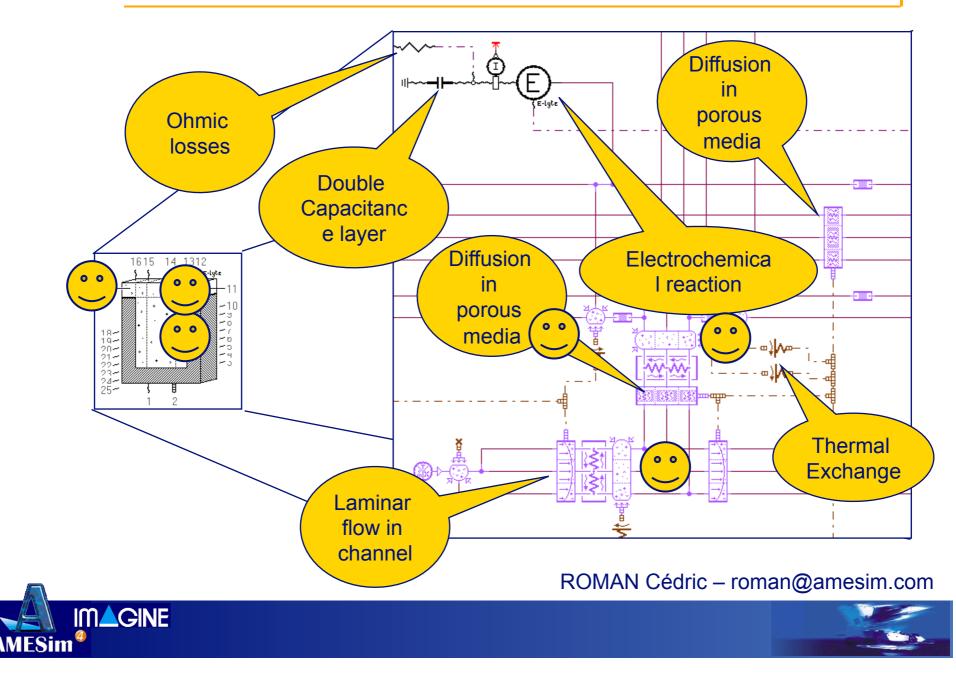


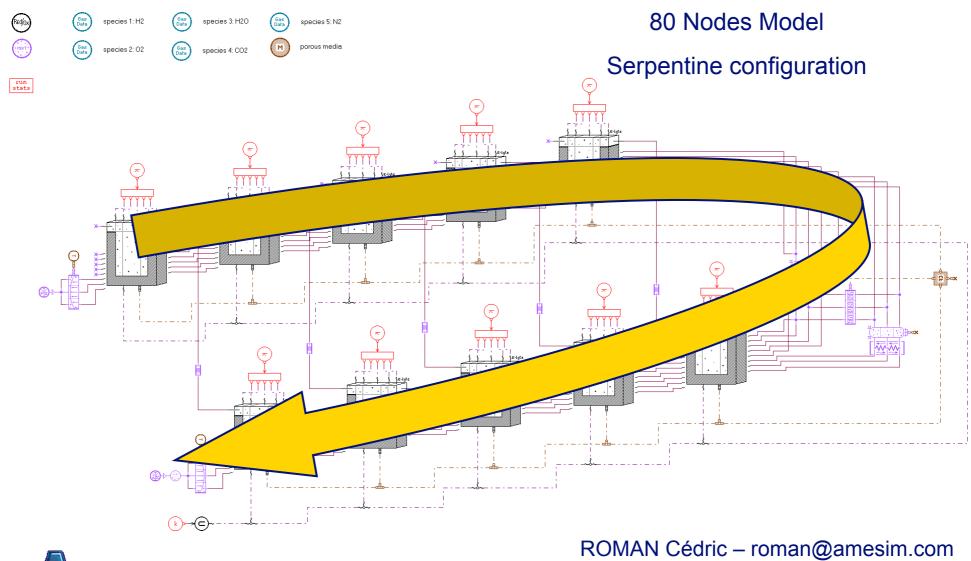
Possible Discretizations







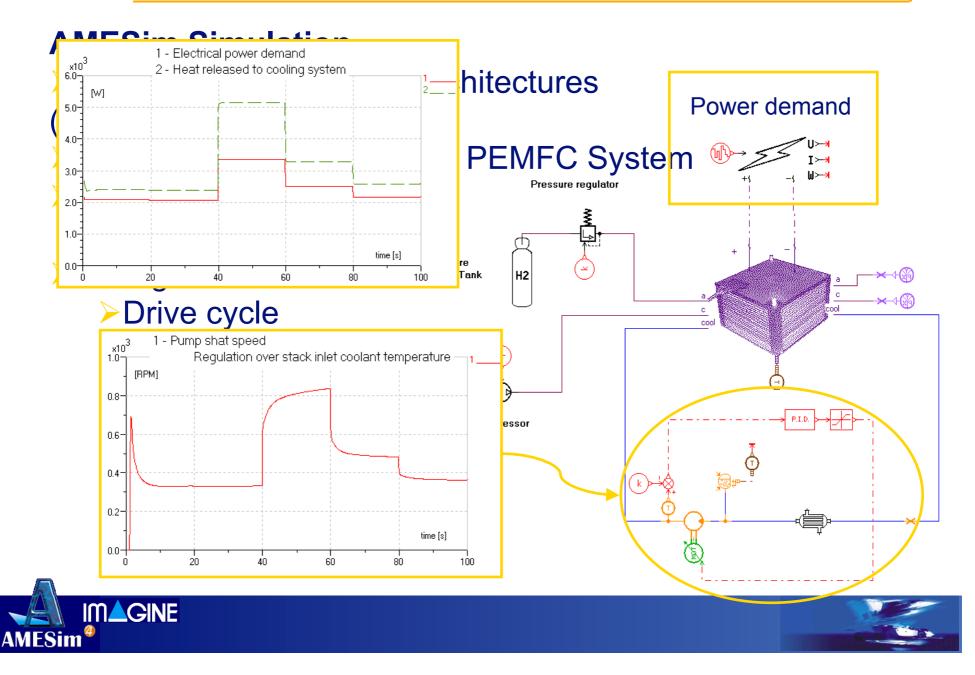








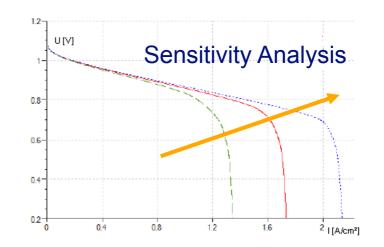
PEMFC system simulation



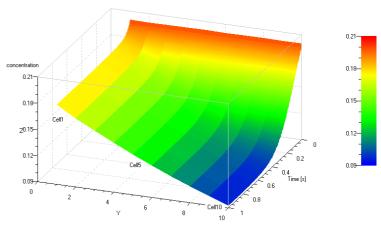
24

PEMFC AMESim model

- Allow quick results
 - Physical model
 - Transient behaviour
 - Gas diffusion efficiency
 - Thermal management
- Robustness & Risk analysis
 - AMESim features
 - Monte-Carlo simulation
 - Design of experiment
 - Optimization











PEMFC AMESim model

Gain Time & Performance (240) Have a better understanding of physics Use all powerfuls AMESim applications Compatible with standard libraries Activity index Linear analysis (Bode, Nyquist, Nichols,...) **Design of Experiment / Optimization Real-time**



